# Interplay between activity, elasticity, and liquid transport in self-contractile biopolymer gels

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Active gels play an important role in biology and in inspiring biomimetic active materials, due to their ability to change shape, size, and create their own morphology. We study a particular class of active gels, generated by polymerizing actin in the presence of cross-linkers and clusters of myosin as molecular motors, which exhibit large contractions. The relevant mechanics for these highly swollen gels is the result of the interplay between activity and liquid flow: gel activity yields a structural reorganization of the gel network and produces a flow of liquid that eventually exits from the gel boundary. This dynamics inherits lengthscales that are typical of the liquid flow processes. The analyses we present provide insights into the contraction dynamics, and they focus on the effects of the geometry on both gel velocity and fluid flow.

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### I. INTRODUCTION

Self-contractile active gels are usually generated by poly-20 merizing actin in the presence of cross-linkers and clusters 21 of myosin as molecular motors [1–7]. The mechanics of ac-22 tive gels presents interesting characteristics: self-contractions 23 generate internal stresses and stiffen the material, thus driving 24 the network into a highly nonlinear, stiffened regime [2]; mor-25 26 phing from flat to curved geometries can be expected when thin disks of active elastic gels are considered [5]; boundaries 27 affect morphing [3]. 28

A distinctive feature of active gels is the fact that the source that drives the system out of equilibrium is local, rather than at the system's boundaries as in passive gels, where boundary tractions and/or fluxes and changes in the chemical equilibrium of the external ambient are the driving forces [8]. From that, we get the definition of active gels as *soft materials in which detailed balance is broken locally* [9].

The first models of active gels are based on a description of the contraction dynamics within the framework of active generalized hydrodynamics, which deal with gel mechanics, liquid transport, and gel activity [5,8–12]. The characteristics of these model are as follows: (i) the liquid flow is described through the mass conservation law and the Stokes equations; (ii) the overall stress in the gel is decomposed in an elastic component, borrowed from the linear elasticity, and an active component, which mimics the active contractile stress generated by the embedded motors; (iii) the overall stress satisfies the balance of forces under a friction force resulting from the relative velocity of the gel and liquid components. The friction force and the active stress make gel mechanics, liquid transport, and gel activity fully coupled.

Hydrodynamic models are very accurate in describing the contraction dynamics at the network mesh scale, and less interested in coupling that dynamics with the nonlinear mechanics of active gels, which is strongly affected by the liquid flow and important when the description of shape transitions in active gels is of interest [5]. More recently, the mechanics of active gels has been at the center of a few theoretical studies, set within the framework of nonlinear mechanics. The interactions between elastic stresses and liquid flow have been investigated in the presence of gel activity, which affects the behavior of the material, and they have been included through different approaches [13–15]. The common point of view is that activity provides structural changes of the network, which induce liquid motion within the gel. Differently from generalized hydrodynamics, gel and liquid motion are modeled using the stress-diffusion theory, a refined version of nonlinear poroelasticity where liquid mass conservation governs liquid transport, and Fick's law takes the place of Darcy's law [16–18].

In [13], a dynamic cross-linking mechanism is introduced that drives an evolution of the mechanical stiffness of the polymeric network and brings the system out of thermodynamic equilibrium. The consequent gradient in the chemical potential of the liquid drives the liquid flow in the active gel. In the approach exploited in [14,15] by some of the authors,

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<sup>75</sup> gel activity acts as a local time-dependent source of strain,
 <sup>76</sup> driven by generalized forces, whose action breaks locally the
 <sup>77</sup> thermodynamic equilibrium of the system.

Here, we describe the active gel state in terms of the liq-78 uid density, the large displacement of the gel, and the active 79 strain, as in [14,15]. In addition, we introduce the relationships 80 between active strains and changes in the natural mesh size 81 of the polymer, defined as the distance between cross-links 82 at zero free-energy; we solve the transient problem for gel 83 disks of different aspect ratio; with reference to those disks, 84 we discuss the regimes of fast and slow liquid transport; we 85 identify the characteristic times of the contraction dynamics; 86 and we study the changes in the overall stress state in gel disks 87 of different aspect ratio. 88

The characteristics of this model are as follows: (i) the 89 liquid flow is described through the mass conservation law, 90 which prescribes the change in liquid concentration in the 91 gel and delivers the liquid velocity relative to the gel; (ii) 92 the total large deformation of the gel is the product of an 93 active component, which mimics the contraction generated by 94 the embedded motors, and an elastic component, following 95 the active strain approach, which has already been success-96 fully exploited to describe morphing and growth in active 97 materials [19–21]; (iii) the overall stress depends on the elastic 98 component through a nonlinear constitutive equation and sat-99 isfies the balance of forces under zero external force; (iv) the 100 generalized forces driving gel activity satisfy a balance equa-101 tion, equivalent to a flow rule for the local time-dependent 102 active strain. 103

Finally, it is worth noting that, in the limit of small deformations, the active strain approach yields an overall stress that is the sum of a passive and an active component, as in generalized hydrodynamics [19].

The goal of the model is describing the interactions between activity, elasticity, and liquid transport through a boundary value problems with initial conditions. Changes in boundary and initial conditions allow us to model a variety of dynamical phenomena and, hopefully, to inspire further experiments to improve the design of the active characteristics of the gel and of its relevant mechanics.

Specifically, we aim to reproduce qualitatively the ex-115 perimental findings presented in [5], where the contraction 116 dynamics of an active gel disk has been followed and de-117 scribed in great detail. In doing so, the analysis of the 118 competitive role of gel contractility and liquid flow in driving 119 the mechanics of the active gel is exploited. It is shown that the 120 shortest lengthscale is relevant for the contraction dynamics, 121 whereas the aspect ratio of the disk (diameter to thickness 122 ratio) affects the evolution of the disk size and the stress 123 distribution. 124

In Sec. II, the basic characteristics of the active gel model 125 are presented and contrasted with those of standard passive 126 gels. In Sec. III, liquid flow, stresses, and gel contractions are 127 introduced, and the equations driving the transient behavior 128 of the disks are presented under the cylindrical symmetry 129 hypotheses. In Sec. IV, the steady states of the active gel 130 are presented. In Sec. V, the regimes of fast and slow liquid 131 transport are identified, and the contraction dynamics of active 132 gel disks of different aspect ratios is studied through a set of 133 numerical experiments. 134

### **II. POLYMER FRACTION AND ACTIVE VOLUME**

Differently from passive polymer gels, active gels have the ability to *reorganize* their mesh, that is, to reduce their natural mesh size by means of motor-induced filaments sliding. A few characteristics of the active and passive gel mechanics are contrasted here through a simple analysis to highlight the key elements that can be described by the macroscopic models of passive and active gels [15,17,18,22–24].

The mechanics of passive polymer gels is commonly 143 studied within the Flory-Rehner model [25,26]. The model 144 assumes the free energy to be the sum of an elastic energy 145 of the network and a mixing energy for the interactions 146 solvent/network. The elastic energy depends on the stretch 147 of the polymer chains from the dry conditions through a 148 nonlinear spring model. The mixing energy depends on the 149 polymer fraction  $\phi$ , that is, the ratio between the volume  $V_p$ 150 occupied by the polymer and the current volume v of the gel: 151

$$\phi = \frac{V_p}{v} \quad \text{with} \quad v = V_p + v_l, \tag{1}$$

where  $v_l$  is the volume of solvent content. Formula (1) is based 152 on the assumption that a given mass of polymer occupies a 153 constant volume  $V_p$ , and any change of the current volume v154 must be entirely due to the solvent volume  $v_l$ . The zero-energy 155 state, that is, the natural state of the gel, corresponds to the 156 dry state ( $\phi = 1$ ). Any change in the solvent content, driven 157 by changes in the chemical potential, stretches the chains, 158 mixes solvent and polymer, and increases the free energy. The 159 balance between the mixing energy, which favors swelling, 160 and the elastic energy, which hampers swelling, yields the 161 thermodynamic equilibrium state. 162

Our active gel model uses the same assumptions for the 163 free energy, but relieves the constraint of a constant polymer 164 volume. The volume of the polymer can vary because of a 165 change of the natural length of the mesh size due to the pulling 166 of molecular motors, and this new volume  $v_a$  is named *active* 167 *volume*. It is worth noting that  $V_p$  and  $v_a$  correspond to the 168 same mass of dry polymer; thus, activity, by changing only 169 the gel volume v, varies the ratio between the polymer mass 170 and the overall gel volume, that is, the effective gel density. 171 Moreover, as liquid is expelled during contraction, gel density 172 increases, a phenomenon called *densification*. For the active 173 gel model, the polymer fraction is given by 174

$$\phi = \frac{v_a}{v} \quad \text{with} \quad v = v_a + v_l. \tag{2}$$

Thus, we may have the same polymer fraction  $\phi$  with different pairs  $v_a, v_l$ : 175

$$\phi = \frac{v_{ao}}{v_{ao} + v_{lo}} = \frac{v_{a1}}{v_{a1} + v_{l1}} \quad \Rightarrow \quad \frac{v_{a1}}{v_{ao}} = \frac{v_{l1}}{v_{lo}}$$
(3)

as  $1/\phi = 1 + v_{l0}/v_{a0} = 1 + v_{l1}/v_{a1}$ . From (3), it follows that 177 a contraction of the polymer network yields a proportional 178 reduction of its solvent content, that is, for  $v_{a1} < v_{a0}$  it holds 179 that  $v_{l1} < v_{l0}$ . For example, if we have  $v_{a0} = 1 \text{ mm}^3$  and 180  $v_{l0} = 1000 \text{ mm}^3$ , we have  $\phi = 1/1001$ . We may have the 181 same polymer fraction  $\phi$ , with a contraction that halves 182 the polymer volume, that is,  $v_{a1} = 0.5 \text{ mm}^3$ , and reduces 183 the solvent content to  $v_{l1} = 500 \text{ mm}^3$ . 184



FIG. 1. The disk is dry at the reference configuration  $\mathcal{B}_d$ , and swollen at the initial one  $\mathcal{B}_o$ . The volume of  $\mathcal{B}_o$  is much larger than that of  $\mathcal{B}_d$  due to liquid content:  $H_o$  and  $2R_o$  are the thickness and diameter of  $\mathcal{B}_o$ , which are  $\lambda_o$  times larger than the corresponding reference lengths. The initial configuration is given by  $x_o = \lambda_o X$ , where the stretch  $\lambda_o$  is determined by the bath's chemical potential.

The natural state of the active gel corresponds to  $\phi = 1$ , 185 and changes in the solvent content can be driven also at con-186 stant chemical potential of the bath: liquid flow is generated by 187 active contraction. We anticipate a key feature of the model: to 188 maintain a steady gel volume, that is, a volume that remains 189 constant in time, motor activity is required. This latter is a 190 distinctive feature of active gels compared to passive ones. 191 Indeed, passive gels under external loads stay in their equi-192 librium state until a change at the system's boundaries occurs. 193 194 On the contrary, active gels are brought out of thermodynamic equilibrium by the action of local molecular motors [8]. 195

This key point inspired us. The model presents a new evolution equation, which describes gel activity; it is driven by a source term representing the local magnitude of motor activity, which brings the system out of equilibrium [9]. This activity in turn generates a solvent flow in the gel: contraction of the polymer mesh, driven by the motors, yields solvent flow towards the boundary of the body, favoring its release.

We conclude this section by writing the relations between 203 the average mesh sizes of the gel and its volumes. Continuing 204 with the example above, the current mesh size  $\xi$  is related 205 to the current gel volume v by  $v \sim \xi^3$ ; likewise, the natural 206 mesh size  $\xi_a$  is related to the active volume  $v_a$  by  $v_a \sim \xi_a^3$ . 207 Thus, the ratio between the two active volumes  $v_{a0}$  and  $v_{a1}$  = 208  $v_{ao}/2$  would scale as  $\xi_{a1}/\xi_{ao} = (1/2)^{1/3} \simeq 0.8$ . Both  $\xi_a$  and  $\xi$ 209 may be very different from the reference mesh size  $\xi_d$  of the 210 dry polymer (before contraction acts), i.e., the passive one, 211 due to activity and liquid flow, as it has been shown in [5] 212 by fluorescence micrographs of a polymerizing and actively 213 contracting actomyosin network (see the cartoon in Fig. 2). 214

## III. LIQUID FLOWS, STRESSES, AND GEL CONTRACTIONS

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<sup>217</sup> The active gel model is formulated in the framework of <sup>218</sup> three-dimensional (3D) continuum mechanics (see [14,15]



FIG. 2. Schematics of the gel: (a) Dry-reference mesh (red) of size  $\xi_d$  with cross-links (blue dots). (b) Dry-contracted mesh: mesh size  $\xi_a$  is reduced with respect to  $\xi_d$ , and cross-link density is higher. (c) Swollen mesh: liquid molecules (light blue dots) swell the dry-contracted mesh: the free energy is proportional to the stretch  $\xi/\xi_a$  between the contracted mesh and the swollen one.

for details), which allows us to set up initial-boundary value 219 problems relevant to describe real experiments. Here, inspired 220 by the experiments in [5], we consider a disklike continuum 221 body. At the initial time, the swollen, flat gel disk  $\mathcal{B}_o$  has 222 radius  $R_o$  and thickness  $H_o$ . Both  $R_o$  and  $H_o$  are  $\lambda_o$  times larger 223 than the radius and thickness of the corresponding dry disk 224  $\mathcal{B}_d$  assumed as a reference configuration of the active gel 225 disk (see Fig. 1). The model describes the state of the gel 226 at any material point  $X \in \mathcal{B}_d$  and time  $\tau \in \mathcal{T}$ , with  $\mathcal{T}$  the 227 time interval, by using the following three state variables: the 228 solvent concentration  $c_d(X, \tau)$  per unit of dry volume ( $[c_d] =$ 229 mol/m<sup>3</sup>), the mechanical displacement  $\mathbf{u}_d(X, \tau)$  ( $[\mathbf{u}_d] = m$ ), 230 and the active strain tensor  $\mathbf{F}_a(X, \tau)$  ( $[\mathbf{F}_a] = 1$ ). To these three 231 state variables of the model, there correspond three balance 232 equations, which control liquid flow, stress state, and active 233 contractions. 234

The current position x of the point X of the gel is given by  $x = X + \mathbf{u}_d(X, \tau)$  and the deformation gradient  $\partial x/\partial X$  is  $\mathbf{F}_d = \mathbf{I} + \nabla \mathbf{u}_d$ . We denote with  $\mathcal{B}_{\tau}$  the current configuration of the gel at time  $\tau$ ; the initial configuration  $\mathcal{B}_o$  is thus given by  $x_o = X + \mathbf{u}_d(X, 0) = \lambda_o X$ , where the stretch  $\lambda_o$  is determined by the bath's chemical potential.

Solvent concentration  $c_d$  and displacement  $\mathbf{u}_d$  are the stan-24 dard state variables of the Flory-Rehner model; the active 242 strain  $\mathbf{F}_a$  is the new variable used to describe the gel contrac-243 tion, that is, the local change of the natural shape of the mesh 244 due to motor activity (see Fig. 2). The tensor  $\mathbf{F}_a$  is the 3D local 245 equivalent of the volume  $v_a$  mentioned in the previous section: 246 given the reference volume element  $dV_d$ , the correspond-247 ing contracted and current volume elements  $dv_a$  and dv are 248 given by 249

$$dv_a = J_a \, dV_d$$
 and  $dv = J_d \, dV_d$ , (4)

with  $J_a = \det \mathbf{F}_a$  and  $J_d = \det \mathbf{F}_d$ . The deformation between 250 the current and the contracted state is measured by the elastic 25 deformation  $\mathbf{F}_e = \mathbf{F}_d \mathbf{F}_a^{-1}$ ; see [19,27]. It is worth noting that 252 no contraction corresponds to  $\mathbf{F}_a = \mathbf{I}$ ,  $J_a = 1$ , and we recover 253 the standard stress-diffusion model of passive gels. Moreover, 254 the time-dependent symmetric tensor  $\mathbf{C}_a = \mathbf{F}_a^T \mathbf{F}_a$  corresponds 255 to the target or natural metric used in [20,21], and the symmet-256 ric tensor  $\mathbf{C}_e = \mathbf{F}_e^T \mathbf{F}_e$  describes the so-called elastic metric, 257 which affects stress distribution in the network [19]. 258 At any point  $X \in \mathcal{B}_d$  and time  $\tau \in \mathcal{T}$ , the solvent content of a volume element is  $dv_l = \Omega c_d dV_d$ , with  $\Omega$  the molar volume of the liquid ( $[\Omega] = m^3/mol$ ). The requirement that the current volume element dv is the sum of the active volume  $dv_a$  plus the liquid volume  $dv_l$ , that is,  $dv = dv_a + dv_l$ , yields an important relation that couples the three state variables of the problem,

$$J_d(X,\tau) = J_a(X,\tau) + \Omega c_d(X,\tau).$$
(5)

Looking at the mesh size, we have the same scaling as in the previous 1D example:  $dv \sim \xi^3$ ,  $dv_a \sim \xi_a^3$ ,  $\xi_a/\xi_d \simeq J_a^{1/3}$ , and  $\xi/\xi_d \simeq J_d^{1/3}$ .

The polymer fraction  $\phi$ , that is, the ratio between  $dv_a$  and dv, is now a function of X and  $\tau$ , and is given by

$$\phi(X,\tau) = \frac{J_a(X,\tau)}{J_d(X,\tau)} = \frac{1}{J_e(X,\tau)} \quad \text{with} \quad J_e = \det \mathbf{F}_e. \quad (6)$$

In the following, we shall study highly swollen active gels 271 whose polymer fraction  $\phi \simeq 10^{-3}$ , while  $J_d$  ranges between 272 1000 and 50. Thus, most of the gel volume is due to liquid 273 content, and given the assumption that the mass of the solid 274 matrix remains constant, the gel densification can be measured 275 by the ratio  $dv_o/dv = J_{do}/J_d$ , where  $dv_o = J_{do} dV_d$  is the 276 volume element of the initial configuration  $\mathcal{B}_o$ . During the 277 contraction, this ratio becomes much larger than 1, as a large 278 volume of liquid is expelled from the gel. This phenomenon 279 has been observed in experiments [5] and is reproduced by our 280 physical model. 281

#### A. Liquid flows

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Any gel contraction deforms the gel and drives liquid flow 283 through it; thus, liquid flows within a moving medium. In 284 the spatial frame, the liquid content  $dv_l$  of a volume ele-285 ment is described by the current concentration c, defined by 286  $dv_l = \Omega c_d dV_d = \Omega c dv$ . From (4), it follows that  $c_d = c J_d$ . 287 Analogously, the gel velocity  $\dot{\mathbf{u}}_d$  is described by the spatial 288 velocity v. The local liquid mass conservation in the current 289 configuration is 290

$$\dot{c} + \operatorname{div}(\mathbf{h} + c \mathbf{v}) = 0$$
 in  $\mathcal{B}_t$ , (7)

and it shows that the solvent flux is the sum of a diffusive component **h** and a convective component c **v**, due to gel velocity **v**, ([**h**] = [c **v**] = mol/m<sup>2</sup> 1/s). Equation (7) can be rewritten as follows:

$$\dot{c} + \operatorname{div}(c \mathbf{v}_l) = 0 \quad \text{with } \mathbf{v}_l = \frac{\mathbf{h}}{c} + \mathbf{v},$$
 (8)

where  $\mathbf{v}_l$  represent the liquid velocity. Hence, the liquid flux  $\mathbf{h}$ depends on the relative liquid velocity to the gel as  $\mathbf{h} = c(\mathbf{v}_l - \mathbf{v})$ . The cartoon in Fig. 3 shows the consequences of Eq. (8) for some values of the relative liquid/gel velocity  $\mathbf{v}_l - \mathbf{v}$ . The liquid volume-rate  $d\dot{v}_l$  through the boundary da of a volume element dv is given by

$$d\dot{v}_l = -\Omega \,\mathbf{h} \cdot \mathbf{n} \, da = -\Omega \, c \, (\mathbf{v}_l - \mathbf{v}) \cdot \mathbf{n} \, da. \tag{9}$$

It holds that  $d\dot{v}_l > 0$  when liquid is uptaken and  $d\dot{v}_l < 0$  when it is expelled. The same volume-rate  $d\dot{v}_l$  can be written in the material frame by using a standard pull-back map; we have

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$$d\dot{v}_l = -\Omega \,\mathbf{h} \cdot \mathbf{n} \, da = -\Omega \,\mathbf{h}_d \cdot \mathbf{m} \, dA_d, \tag{10}$$



FIG. 3. Given a point (circle) on the boundary (vertical thick line), the current flux **h** through the boundary (blue arrow) depends on the relative velocity  $(\mathbf{v}_l - \mathbf{v})$ . The cartoon shows four cases with different  $\mathbf{v}_l$  (red arrow), whose outcome ranges from zero flux (top) to a very large flux (bottom).

with **n** and **m** the unit normals to the area elements da and  $_{304}^{304}$ , respectively. Equation (10) yields the definition of the reference flux  $\mathbf{h}_d = J \mathbf{F}^{-1} \mathbf{h}$ .

Also, the local liquid mass conservation (7), written in the current configuration, can be pulled back from  $\mathcal{B}_t$  to  $\mathcal{B}_d$ : the corresponding liquid mass conservation written in the material frame  $\mathcal{B}_d$  is given by 310

$$\dot{c}_d + \operatorname{div} \mathbf{h}_d = 0 \quad \text{in} \quad \mathcal{B}_d. \tag{11}$$

Equation (11) is the one we shall use and solve in our model. It is worth noting that by writing the liquid mass conservation in the material frame, it could not be noticed at a glance that the liquid flux  $\mathbf{h}_d$  is the sum of a diffusive term plus a convective one. 314

#### B. Stresses and active contractions

The overall stress in the current configuration is measured by the Cauchy stress tensor **T**, which gives the force **Tn** per unit current area *da*. To **T** there corresponds a nominal stress  $\mathbf{S}_d = \mathbf{T}\mathbf{F}_d^{\star}/J$ , which gives the force  $\mathbf{S}_d\mathbf{m}$  per unit reference area *dA* [therein,  $\mathbf{F}_d^{\star} = (\mathbf{F}_d^T)^{-1}$ ]. The balance equation of forces in the reference configuration  $\mathcal{B}_d$  is written in terms of  $\mathbf{S}_d$  as  $\mathbf{S}_d = \mathbf{T}\mathbf{F}_d^{\star}/J$ 

div 
$$\mathbf{S}_d = \mathbf{0}$$
 in  $\mathcal{B}_d$  and  $\mathbf{S}_d \mathbf{m} = \mathbf{0}$  on  $\partial \mathcal{B}_d$ . (12)

The right side of (12) is zero because we are neglecting inertial forces (as timescales associated with diffusion and activity are considerably longer than those associated with inertia). The right side of (12) is zero because we are assuming that the boundary pressure exerted by the liquid in the bath on the gel is negligible, and we do not have any other external boundary tractions.

Balance of forces holds at any time *t* and, when the liquid flux  $\mathbf{h} = \mathbf{0}$ , characterizes the thermodynamic equilibrium in passive gels. In active gels we have one more balance equation describing the contraction dynamics. It produces a 334

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dissipative dynamics in the form of a flow rule for the local time-dependent active strain  $\mathbf{F}_a$  as

$$\dot{\mathbf{F}}_a = \mathbf{M}^{-1}\{[\mathbf{B} - \mathbf{E}_{\rm sh}(\mathbf{F}, c_d)]\}\mathbf{F}_a,\tag{13}$$

where the generalized force **B** mimics the action of the molecular motors, and the Eshelby tensor  $\mathbf{E}_{sh}$  brings in the model the effect of the chemomechanical state of the body. Finally, the power density dissipated in the system due to active contraction is  $\mathbf{M}\dot{\mathbf{F}}_{a} \cdot \dot{\mathbf{F}}_{a}$ , and the *dissipation tensor* **M** is assumed to be positive-definite (to get a positive dissipation power density) and diagonal.

#### C. Model equations under cylindrical symmetry

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We exploit the cylindrical symmetry that greatly simplifies 345 the evolution equations of the problem; thus, the reference 346 disk  $\mathcal{B}_d$  is represented by its vertical cross section  $\mathcal{S}_d$  spanned 347 by the radial coordinate  $r \in (0, R_d)$  and the vertical one  $z \in$ 348 349  $(0, H_d)$ . With this, the displacement  $\mathbf{u}_d$  has two nonzero components: the radial u and the vertical w component; within 350 the class of tensors  $\mathbf{F}_a$ , which are cylindrically symmetric, 351 we choose a diagonal one and write  $\mathbf{F}_a = \text{diag}(\gamma_r, \gamma_{\theta}, \gamma_z)$ . 352 The consequence of this choice is that our active contraction 353 provides a change in the natural mesh size that acts as a 354 local time-dependent source of volumetric and linear strains, 355 whereas shear strains are neglected. 356

The state variables of the problem are reduced to the fol-357 lowing six scalar fields: the solvent concentration  $c_d$ , the two 358 displacements (u, w), and the three contractions  $(\gamma_r, \gamma_{\theta}, \gamma_z)$ ; 359 each field is a function of the coordinates (r, z) and the time  $\tau$ . 360 Moreover, we assume that the derivatives  $u_{,z}$  and  $w_{,r}$  are zero, 361 that is, we neglect any possible small shearing between the 362 vertical and radial directions. It follows that the deformation 363 gradient  $\mathbf{F}_d$  reduces to  $\mathbf{F}_d = \text{diag}(\lambda_r, \lambda_\theta, \lambda_z)$  with the radial, 364 hoop, and vertical deformations defined as 365

$$\lambda_r = 1 + u_{,r}, \quad \lambda_\theta = 1 + u/r, \quad \lambda_z = 1 + w_{,z}, \quad (14)$$

respectively. Under the symmetry assumption, the volumetric
 constraint (5) takes the form

$$\lambda_r \lambda_\theta \lambda_z = 1 + \Omega \, c_d. \tag{15}$$

The state of the active gel is ruled by the set of balance equations introduced above. Under the cylindrical symmetry hypotheses, Eq. (11) reduces to

$$-\dot{c}_d = h_{r,r} + \frac{h_r}{r} + h_{z,z}, \quad [3mm]$$
 (16)

where  $h_r$  and  $h_z$  are the radial and vertical components of the solvent flux. So, the liquid volume rate through the lateral surface of the disk is  $2\pi R_d \Omega h_r(R_d, z) dz$ , whereas the liquid volume rate through the top face of the disk is  $2\pi r \Omega h_z(r, H_d) dr$ . Equations (12) reduce to

$$s_{r,r} + \frac{s_r - s_{\theta}}{r} = 0$$
 and  $s_{z,z} = 0$ , (17)

where  $s_r$ ,  $s_{\theta}$ , and  $s_z$  are the radial, hoop, and vertical components of the nominal stress (also called symmetric Piola stress), that is, the stress components on an area element  $dA_d$ orthogonal to the radial direction, to the azimuthal direction, and to the vertical direction.

Fluxes  $h_r$  and  $h_z$ , chemical potential  $\mu$ , and stresses  $s_r$ , 381  $s_{\theta}$ , and  $s_z$  are related to the stretches  $\lambda_i$  and the contractions 382  $\gamma_i$  (*i* = *r*,  $\theta$ , *z*) by constitutive equations, whose derivation is 383 fully described in several texts and papers (see [16,18,27]). 384 Shortly, liquid transport in the gel is described by a kinetic 385 law, based on the assumption that the liquid molecules move 386 across the gel pores following Fick's law (linear dependence 387 on the chemical potential gradient): 388

$$h_r = -\frac{D c_d}{R T \lambda_r^2} \mu_{,r}$$
 and  $h_z = -\frac{D c_d}{R T \lambda_z^2} \mu_{,z}$ , (18)

where *D* is the diffusion coefficient, which has been assumed to be the same in the radial and vertical directions, *R* and *T* are the gas constant and the temperature, respectively, and  $\mu = 10^{-10} \mu (J_e, p)$  is the chemical potential of the solvent in the gel:  $10^{-10} \mu (J_e, p)$ 

$$\mu = R T g(J_e) + \Omega p, \quad J_e = \det \mathbf{F}_e = \frac{J_d}{J_a}, \quad (19)$$

with

$$g(J_e) = \left[\log\left(\frac{J_e - 1}{J_e}\right) + \frac{1}{J_e} + \frac{\chi}{J_e^2}\right].$$
 (20)

Therein, the parameter  $\chi$  is the nondimensional disaffinity 394 parameter, which controls the attraction between liquid and 395 network, and the pressure field p is the Lagrangian mul-396 tiplier of the constraint  $J_d = J_a + \Omega c_d$  [Eq. (5)] [22]. The 397 characteristic time  $l^2/D = \tau_d$  of the liquid transport, with l398 a characteristic length of the problem, will be compared with 399 the characteristic times brought in the model by contraction 400 dynamics to identify different regimes. 40

Finally, the overall stresses are given by constitutive equations of the form 402

$$s_{r} = G \lambda_{r} \frac{\gamma_{\theta} \gamma_{z}}{\gamma_{r}} - p \lambda_{\theta} \lambda_{z},$$

$$s_{\theta} = G \lambda_{\theta} \frac{\gamma_{r} \gamma_{z}}{\gamma_{\theta}} - p \lambda_{r} \lambda_{z},$$

$$s_{z} = G \lambda_{z} \frac{\gamma_{r} \gamma_{\theta}}{\gamma_{z}} - p \lambda_{r} \lambda_{\theta},$$
(21)

where *G* is the shear modulus of the dry polymer network ([*G*] =J/m<sup>3</sup>). The corresponding Cauchy stresses are  $\sigma_r = \frac{404}{s_r/\lambda_{\theta}\lambda_z}$ ,  $\sigma_{\theta} = \frac{s_{\theta}}{\lambda_r\lambda_z}$ , and  $\sigma_z = \frac{s_z}{\lambda_{\theta}\lambda_r}$ .

Finally, Eq. (13) specializes to three scalar equations, which deliver the flow rules for the active contractions  $\gamma_i$  408  $(i = r, \theta, z)$  [28]:

$$\dot{\gamma}_{r} = \frac{1}{\eta_{r}} (\beta_{r} - E_{r}) \gamma_{r},$$
  
$$\dot{\gamma}_{\theta} = \frac{1}{\eta_{\theta}} (\beta_{\theta} - E_{\theta}) \gamma_{\theta},$$
  
$$\dot{\gamma}_{z} = \frac{1}{\eta_{z}} (\beta_{z} - E_{z}) \gamma_{z}.$$
 (22)

These equations show that flow rules are driven by  $(\beta_i - E_i)$  410 ( $i = r, \theta, z$ ), that is, by the difference between the generalized 411 forces  $\beta_i$  and the components  $E_i$  of the Eshelby tensor, which 412 depends constitutively on the chemomechanical state of the 413 gel. We assume  $\beta_i(X, \tau) = \beta(\tau)$ , corresponding to assuming 414 an isotropic and homogeneous distribution of motors in the 415 gel, and we view it as the control parameter of the contraction 416

<sup>417</sup> process. On the contrary, we cannot control the components <sup>418</sup>  $E_i$ , which are in general neither homogeneous nor constant <sup>419</sup> and, within the Flory-Rehner thermodynamics, depend on the <sup>420</sup> state of the gel as

$$E_i = e_y - J_d \sigma_i \quad (i = r, \theta, z)$$
(23)

421 with

$$e_y = \frac{RT}{\Omega} J_a F(\mathbf{C}_e) - c_d \,\mu(J_e, p). \tag{24}$$

The function  $F(\mathbf{C}_e)$  is the dimensionless free-energy density per unit natural volume, and it reads  $F(\mathbf{C}_e) = f_c(J_e) + m f_e(\mathbf{C}_e)$ , with  $f_c$  and  $f_e$  the dimensionless mixing and elastic free-energy, where  $m = G\Omega/RT$  is the ratio between the elastic energy and the mixing energy:

$$f_c(J_e) = (J_e - 1)\log\left(1 - \frac{1}{J_e}\right) + \chi\left(1 - \frac{1}{J_e}\right),$$
  
$$f_e(\mathbf{C}_e) = \frac{1}{2}(\operatorname{tr}\mathbf{C}_e - 3).$$
(25)

Equations (22)–(25) show that the interplay between activity, elasticity, and liquid transport depends on the effective controls ( $\beta - E_i$ ); in general, the dissipation constants  $\eta_i$  can be different in the three directions and can bring in the model more than one characteristic time  $\tau_{\eta_i} = \eta_i / RT / \Omega$ ; large dissipation constants yield small contraction time rates ( $\dot{\gamma}_r$ ,  $\dot{\gamma}_\vartheta$ ,  $\dot{\gamma}_z$ ), under the same effective input.

We assume that the disk is not constrained, nor loaded, the entire disk boundary is permeable, and chemical equilibrium holds at the boundary, that is,

$$\mu = \mu_e \quad \text{on} \quad \partial \mathcal{S}_d, \tag{26}$$

where  $\mu_e$  is the difference between the chemical potential of the bath and that of pure water ( $\mu_e = 0$  corresponds to a pure water bath). Finally, the initial conditions for the displacements u, w, the concentration  $c_d$ , and the contractions  $\chi_{i}$  ( $i = r, \theta, z$ ) are the following:

$$u = (\lambda_o - 1) r, \quad w = (\lambda_o - 1) z, \quad c_d = c_{do}, \quad \gamma_i = 1,$$
(27)

<sup>442</sup> corresponding to the deformation  $f_o(X) = \lambda_o X$  for any  $X \in \mathcal{B}_d$  from  $\mathcal{B}_d$  to  $\mathcal{B}_0$  (see Fig. 1).

## 444 IV. INITIAL AND FINAL EQUILIBRIUM STATES

The controls  $\mu_e$  and  $\beta$  trigger contraction-liquid transport dynamics between the initial and the final state (see Fig. 4). We assume that both  $\mu_e$  and  $\beta$  have a characteristic evolution dynamics from their initial values ( $\mu_0$ ,  $\beta_0$ ) to their final values ( $\mu_1$ ,  $\beta_1$ ), described by the following time laws:

$$\mu_{e} = \mu_{e}(\tau) = \mu_{0} + (\mu_{1} - \mu_{0}) \, \mathrm{s}(\tau/\tau_{\mu}),$$
  
$$\beta = \beta(\tau) = \beta_{0} + (\beta_{1} - \beta_{0}) \, \mathrm{s}(\tau/\tau_{\beta}), \qquad (28)$$

where  $s(\cdot)$  is a smoothed step function [29] running from 0 to 1 in the interval (0,1), and  $\tau_{\mu}$  and  $\tau_{\beta}$  are characteristic times [30], which have been tuned to match the results presented in [5]; see Table I. For the motors, the characteristic time depends on the binding/unbinding kinetics of the motors to the actin filaments, whereas for the chemical potential, the



FIG. 4.  $\beta$  goes from  $\beta_0$  to  $\beta_1$  in  $\tau_{\beta} = 20$  s (dashed and solid red lines);  $\mu$  stays constant in scenario (a) and goes from  $\mu_0 = 0$  to  $\mu_1$  in  $\tau_{\mu} = 100$  s (solid blue).  $\beta$  axis at left,  $\mu$  axis at right.

characteristic time reflects the mixing kinetic of possibly free biopolymer chains and the liquid in the bath.

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The initial state and the final one are *equilibrium states*, that is,  $\mathbf{h}_d = \mathbf{0}$ , which implies  $\dot{c}_d = 0$  and  $\dot{\gamma}_i = 0$  ( $i = r, \theta, z$ ).

We assume that at the initial and final equilibrium states,  $\mathbf{F}_d$  and  $\mathbf{F}_a$  are uniform and spherical, that is,  $\mathbf{F}_d = \lambda \mathbf{I}$ ,  $\mathbf{F}_a = 461$   $\gamma \mathbf{I}$ , and that the overall stress is null. With this, and with Eqs. (21), (19), and (23), we can represent the chemical potential and the Eshelby components at those equilibrium states as functions of  $J_a = \gamma^3$  and  $J_d = \lambda^3$ :

$$\mu = \mu(J_d/J_a) = \mu(J_e)$$
 and  $E_i = e_y(J_a, J_e)$ . (29)

Moreover, the equilibrium states are guaranteed by constant and homogeneous chemical potential  $\mu_e$  and bulk source  $\beta$  467 such that 468

$$\mu_e = \mu$$
 and  $\beta = E_i$ . (30)

Equations (29) and (30) deliver the relation between the pair  $(J_a, J_d)$  and the pair  $(\mu_e, \beta)$  which must hold at the equilibrium states: 469

$$\mu_e = \mu(J_e)$$
 and  $\beta = e_y(J_a, J_e).$  (31)

TABLE I. Material and geometrical parameters.

Shear modulus	G = 135  Pa
Flory parameter	$\chi = 0.4$
Water molar volume	$\Omega = 1.8 \times 10^{-5} \text{ m}^3/\text{mol}$
Temperature	T = 293  K
Energy ratio	$m = G \Omega/R T = 1 \times 10^{-6}$
Diffusivity	$D = 1 \times 10^{-3} \text{ m}^2/\text{s}$
Dissipation	$\eta = 1 \times 10^5$ Pa s
Initial radius	$R_o = 1500 \mu \text{m}$
Initial swollen volume and stretch ratio	$J_o = 1000, \ \lambda_o = 10$
Initial aspect ratio	$AR = 2R_o/H_o = 20-40$
Initial thickness	$H_o = 150-75 \ \mu \text{m}$
Final volume/initial volume	$J_{a1} = 0.05$
Control time for $\beta$	$\tau_{\beta} = 20 \text{ s}$
Control time for $\mu$	$\tau_{\mu} = 100 \text{ s}$
•	

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We label  $(J_{d0}, J_{a0})$  the pair corresponding to the initial equilibrium state and  $(J_{d1}, J_{a1})$  the pair corresponding to the final state; the same labels hold for all the other quantities.

#### 1. Material parameters

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The values assigned to the initial thickness and aspect 476 ratio (AR) have been prompted by [5], and the successive 477 parametric analyses always consider values of AR and  $H_0$  not 478 too far from the initial ones. The discrepancy between our 479 value for the shear modulus G and the value reported in [5] 480 is due to the fact that the former is the shear modulus at dry 481 conditions, while the latter is the effective shear modulus  $G_{\rm eff}$ 482 measured at the swollen state, with  $G_{\rm eff} \simeq G/J_{d0}^{1/3}$ . We set the 483 diffusivity constant D and the dissipation  $\eta_r = \eta_{\theta} = \eta_z = \eta$  in 484 order to get a time evolution from  $\mathcal{B}_o$  to  $\mathcal{B}_1$  similar to that taken 485 by the real disk to reach a mechanically stable state (steady 486 state), that is,  $\sim 200$  s. With this, we set the characteristic time 487  $\tau_n$ , leaving  $\tau_d$  free to get different values, depending on  $H_o$ , 488 which are in any case always higher than  $\tau_n$  (see Table I for 489 the complete list of material parameters). 490

#### 2. Initial state

We assume a fully swollen state as the initial state of the gel, characterized by a not contracted mesh size  $\xi_a$  equal to the reference mesh size  $\xi_d$ . From an experimental point of view, it means that self-contraction and liquid release are going to be initiated; from the modeling point of view, it means that the active gel is still not contracted and is in its thermodynamic equilibrium, that is,

$$\mu_e(0) = \mu_0 = 0$$
 J/mol and  $J_{a0} = 1.$  (32)

<sup>499</sup> By putting these values in Eqs. (31), we find the initial change <sup>500</sup> in volume  $J_{d0} = J_{e0} = \lambda_0^3$  of the gel and the initial value  $\beta_0$ <sup>501</sup> of the generalized force which maintains that initial state. <sup>502</sup> Specifically, Eqs. (31) take the form

$$0 = \mu(J_{d0}/J_{a0}) \quad \text{and} \quad \beta_0 = e_y(J_{a0}, J_{e0}). \tag{33}$$

<sup>503</sup> The zero stress condition at the initial time delivers  $p_0 = G/\lambda_o$ . With this, the constitutive Eqs. (19) and (20) for the <sup>505</sup> chemical potential and Eq. (33) deliver

$$0 = \left[ \log \left( 1 - \frac{1}{\lambda_0^3} \right) + \frac{1}{\lambda_0^3} + \frac{\chi}{\lambda_0^6} \right] + \frac{m}{\lambda_0}.$$
 (34)

Equation (34) can be solved for  $\lambda_0$ , and Eq. (33) determines the initial value  $\beta_0$  which the control has to get to guarantee null contraction ( $\xi_a = \xi_d$ ) and the free swelling stretch  $\lambda_0$ :

$$\frac{\Omega}{RT}\beta_0 = (\lambda_0^3 - 1)\left(\frac{\lambda_0^3 - 1}{\lambda_0^6}\chi - \frac{1}{\lambda_0^3}\right) + m\left(\frac{1}{\lambda_0} + \frac{\lambda_0^2}{2} - \frac{3}{2}\right).$$
(35)

It is worth noting that Eq. (34) is standard in stress-diffusion theories based on Flory-Rehner thermodynamics [25,26]; it is easy to verify that, given  $\mu_0$ , the free-swelling stretch  $\lambda_0$ increases as *m* decreases. On the contrary, Eq. (35) does not belong to standard stress-diffusion theory, and it is peculiar to the present augmented model. The initial values of  $J_d$ ,  $J_e$ ,  $c_d$ , p, and  $\beta$ , corresponding to the material parameter in Table I, can be easily evaluated. In particular, we get  $J_{d0} = 1000$ .

#### 3. Final states

We consider two different scenarios: (a) where only a change in the generalized force drives the active contractions and liquid transport, that is,  $\beta_1 \neq \beta_0$  and  $\mu_1 = \mu_0$ ; (b) where also a change in the chemical potential of the bath drives the active contractions and liquid transport, that is,  $\beta_1 \neq \beta_0$  and  $\mu_1 = \mu_0$ ; (b) where  $\mu_1 \neq \mu_0$ .

The differences between the two scenarios are noteworthy. 525 Indeed, in passive gels the input that drives the system out 526 of equilibrium is at the system's boundaries, that is, a change 527 of the chemical potential in the bath starts liquid transport. 528 On the contrary, a distinctive feature of active gels is the fact 529 that the input that drives the system out of equilibrium is 530 local. Through the analysis of the two scenarios, we compare 531 dynamics due to only local input, that is, a change in the 532 generalized force, and to both local and boundary input, that 533 is, a change in both the generalized force and the chemical 534 potential of the bath. 535

In both the scenarios, however, and in accordance with the 536 experiments in [5], we assume that at the final state the mesh 537 is contracted by  $\xi_a/\xi_d = J_{a1}^{1/3} \simeq 0.38$  with respect to the dry 538 mesh size, that is,  $J_{a1} = (\xi_a/\xi_d)^3 = 0.05$ . The estimation of 539 the final value  $J_{a1}$  allows us, within the model, to estimate the 540 final value  $\beta_1$  of the generalized force, as is shown below by 541 describing step-by-step the procedure to infer those data from 542 the equations of the model. 543

*Scenario a (fluid flow induced by active contractility).* We assume 544

$$\mu_1 = \mu_0 = 0 \text{ J/mol}, \quad J_{a1} = 0.05,$$
 (36)

and we put these values in Eqs. (31) to obtain the final swelling ratio  $J_{d1}$  and the generalized force  $\beta_1$ . Specifically, the two equations take the form 548

$$0 = \mu(J_{d1}/J_{a1}) \quad \text{and} \quad \beta_1 = e_y(J_{a1}, J_{e1}). \tag{37}$$

With our data, we find  $J_{d1} = 50$ . Comparing this value with the change in volume delivered under the same chemical conditions, that is,  $J_{d0} = 1000$ , we can conclude that, due to self-contraction, an effective bulk stiffening is predicted by the model, as has already been recognized as crucial in other works [10].

Scenario b (fluid flow generated by the active contractility 555 and changes in the chemical potential of the liquid bath). 556 Typically, in the experiments, the chemical potential of the 557 bath is not controlled. While previously assumed constant 558 [see (a)], it is possible that chains, small fragments, and even 559 monomers can be broken from the gel and released into the 560 solution upon contraction of the gel, by changing the chemical 56 potential of the bath [31]. This motivated our choice to study 562 the impact of a change in  $\mu_e$  on the contraction dynamics. 563

We assume that at the final equilibrium state,  $J_{d1}$  is half the value of case (a), while  $J_{a1}$  is the same as before, that is,

$$J_{d1} = 25, \quad J_{a1} = 0.05. \tag{38}$$

TABLE II. Data about the aspect ratios; values of  $R_o$  and  $H_o$  are in mm.

Constant $R_o$ Constant $H_o$ $H_o(R_o = 1.5)$ $R_o(H_o = 0.1)$		AR	
0.15	10	20	
0.12	1.25	20	
0.1	1.50	30	
0.086	1.75	35	
0.075	2.0	40	
0.066	2.25	45	

By putting these values in Eqs. (31), we obtain the pair 566  $(\mu_1, \beta_1)$ . Specifically, the two equations take the form 56

$$\mu_1 = \mu(J_{d1}/J_{a1})$$
 and  $\beta_1 = e_y(J_{a1}, J_{e1}).$  (39)

Of course, other choices would be possible; for example, apart 568 from setting different values for  $J_{d1}$ , we could first set  $\mu_1$  and 569 then determine  $J_{d1}$  from Eqs. (31). What we aimed to remark 570 is that the same value of  $\beta_1$  can deliver a quite different value 571 of the final change in volume  $J_{d1}$  of the disk (25 versus 50) 572 when liquid transport and release is driven by both the mesh 573 contraction and the change in the chemical conditions of the 574 bath 575

#### V. CONTRACTION DYNAMICS

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Gel activity does not have any characteristic lengths, since 577 motor activity is assumed to be homogeneous across the sys-578 tem. However, contraction dynamics inherits the characteristic 579 length of the dynamic of liquid transport. The disks built and 580 tested in [5] represent a good basis for a pilot study aimed to 581 discuss the relations between the two dynamics in terms of 582 the key geometrical parameter, which is the aspect ratio of the 583 disks. 584

We carried on the analysis by either changing the disk ini-585 tial thickness  $H_o$ , for a fixed initial disk radius  $R_o = 1.5$  mm, 586 or by varying the disk initial radius at a fixed thickness  $H_o =$ 587 0.10 mm. The investigated range of parameter AR is described 588 in Table II: it goes from disks of initial aspect ratio 20 (thick 589 disks) to disks of initial aspect ratio 45 (thin disks). 590

We show the results obtained for gel disks that contract due 591 to motor only [so-called scenario (a)]. All the experiments 592 start with  $J_{d0} = 1000$ , i.e., at a highly swollen initial state, 593 and  $J_{a0} = 1$ , and they evolve towards their final steady values 594  $J_{d1} = 50$  and  $J_{a1} = 0.05$ . As stated above, these values corre-595 spond to a reduction in mesh size  $= \xi_{a1}/\xi_{ao} = 0.05^{1/3} = 0.38$ , 596 where  $\xi_{a1}$  represents the final mesh size, and, as stated above, 597 we consider the final state to be stress-free. 598

In the regime under study, the system reaches its final steady state after  $\tau_1 \simeq 200$  s, that is, we have  $\tau_\beta \ll \tau_1$  and 600 the dynamics is ruled by the redistribution of water across 601 the gel mesh until its eventual expulsion through the disk 602 boundary. 603

#### A. Diffusion-limited regime

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Given the equations of the model, there are different 605 characteristic times whose values have an influence on the 606



FIG. 5. Plot of  $\overline{J}_d$  (solid) and  $\overline{J}_a$  (dashed) vs time for different values of AR; disk geometry is given in the first column of Table II. Being  $\tau_{\eta} \ll \tau_{\beta}$ , all the  $\bar{J}_a$  curves (dashed) are superimposed, as  $\bar{J}_a$ evolves at the same pace of  $\beta$ , and this evolution is not affected by AR. The  $\bar{J}_d$  curves (solid) depends strongly on AR, and the thicker the disk, the slower the volume change. This is a consequence of the fact that the liquid must exit through the boundary, and the thickness is the important geometric parameter within our range of AR.

different solution regimes. In particular, the characteristic time 607  $\tau_{\eta}$  which governs mesh contraction is not size-dependent, 608 being  $\tau_\eta \propto \eta \, \Omega/RT$ , while the characteristic time  $\tau_d$  which 609 governs liquid transport has a length scale, which for our 610 geometries is the current height H, that is,  $\tau_d \propto H^2/D$ . Given 611 our choice of  $\eta$ , we have  $\tau_{\eta} \simeq 10^{-3}$  s; the estimation of a value 612 for  $\tau_d$  is much more difficult because of the large size-change experienced by the disks during contraction. 614

Our experiments shows that, for our choice of parameters and geometry, the contraction dynamics is *diffusion-limited*, as is affected by the lengthscale. The opposite regime, the socalled *motor-limited* regime, can be realized when  $\tau_d \ll \tau_n$ . 618 The simplest way to discuss the different regimes is through 619 the analysis of the flow rule for  $J_a$ , which can be easily derived 620 from Eqs. (22)–(24). Cylindrical symmetry implies 621

$$J_a = \gamma_r \gamma_\theta \gamma_z$$
 and  $\dot{J}_a = J_a \left( \frac{\dot{\gamma}_r}{\gamma_r} + \frac{\dot{\gamma}_\theta}{\gamma_\theta} + \frac{\dot{\gamma}_z}{\gamma_z} \right).$  (40)

With this, the flow rule for  $J_a$  can be derived from those for  $\gamma_i$ 622 by Eqs. (22), and it takes the form 623

$$\dot{J}_a = \frac{1}{\eta} [3(\beta - e_y) + J_d \operatorname{tr} \mathbf{T}] J_a.$$
(41)

Equation (41) and the equation governing the dynamics of 624 diffusion allow us to discuss some of the evidences of our 625 numerical experiments. 626

To discuss contraction dynamics, we define the averages 627  $\bar{J}_d(\tau)$  and  $\bar{J}_a(\tau)$  of  $J_d(r, z, \tau)$  and  $J_a(r, z, \tau)$ , respectively, 628 which well represent the main features of the phenomenon 629 under study, and give a global glance at the contraction dy-630 namics. Due to the cylindrical symmetry of the system, both 631 averages are evaluated on the two-dimensional domain  $\mathcal{S}_d$  of 632 area  $R_d \cdot H_d$ . 633

In Fig. 5, we plot  $\bar{J}_a$  (dashed) and  $\bar{J}_d$  (solid) versus time for 634 different values of AR; the figure shows two major findings. 635



FIG. 6. Plane  $(\bar{J}_d, \bar{J}_a)$ : evolution path at constant radius  $R_o =$  1.5 mm for different values of AR; disk geometry is given in the first column of Table II. Lower AR correspond to the evolution path far from equilibrium; higher AR corresponds to paths that tend to the quasistatic stress (dashed line).

First, all the curves for  $\bar{J}_a$  are superimposed, as  $\tau_\eta \ll \tau_\beta$ , that is, the evolution of  $\beta$  is slow with respect to the characteristic time  $\tau_\eta$ , and  $\bar{J}_a(\tau)$  has the same dynamics of  $\beta(\tau)$ ; in particular, the evolution of  $\bar{J}_a$  can be approximated as a sequence of equilibrium problems, which depend on  $\beta$ . Moreover, as contraction is a local mechanism, this dynamics is much faster than diffusion, and it is not affected by AR.

Secondly, the curves for  $\bar{J}_d$ , representing the volume change, strongly depend on AR, and the thicker the disk, the slower the volume change. This is a consequence of the fact that the liquid must exit through the boundary, and for the range of AR under investigation, the thickness is the important geometric parameter.

#### **B.** Dynamics in the plane $(\bar{J}_d, \bar{J}_a)$

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We now focus on the evolution paths in the plane  $(\bar{J}_d, \bar{J}_a)$ for scenario (a), that is,  $\mu_e = \mu_o = \text{const.}$  In this plane, a quasistatic stress-free path is represented by a straight line at constant  $\bar{J}_e = \bar{J}_d / \bar{J}_a$ , and the dashed line in Figs. 6 and 7. This path corresponds to a sequence of equilibrium states where the current swollen volume  $\bar{J}_d$  corresponds to a free swelling for a dry mesh whose current natural volume is  $\bar{J}_a$ .

657 Due to the choices made in Table I, which yields a diffusion-limited regime, liquid transport is affected by the 658 lengthscale. Thus, thinner disks (higher AR) show an evo-659 lution in the plane that is closer to the stress-free path, that 660 is, under the same contraction dynamics, liquid transport is 661 faster for these disks, which can quickly recover the original 662 stress-free state. On the contrary, for thicker disks (lower AR), 663 the evolution path is very far from the quasistatic regime: 664 namely, motor-induced contraction is faster than the water 665 transport across the gel mesh, which makes the thick gels 666 highly stressed during their evolution. 667

We investigated the evolution paths for different AR for varying  $H_o$  at constant  $R_o$  (Fig. 6) and varying  $R_o$  at constant  $H_o$  (Fig. 7). In the first case, Fig. 6 shows that by increasing the thickness  $H_o$ , that is, the characteristic lengthscale across



FIG. 7. Plane  $(\bar{J}_d, \bar{J}_a)$ : evolution path at constant thickness  $H_o = 0.1$  mm for different values of AR; disk geometry is given in the second column of Table II. All the paths are superimposed and the master curve is the one corresponding to AR = 30 in Fig. 6.

which water flows, it increases the characteristic timescale of water transport (from yellow to blue solid lines). As  $\tau_{\eta} \gg \tau_d$  for any values of  $H_o$ , the quasistatic path is never realized; however, the thinner the disk is, the closer is the evolution path to the quasistatic one. 676

To confirm our expectations that the important lengthscale for water exit is  $H_o$ , we also studied disk geometries having constant thickness and varying radius. Figure 7 shows the results for the same range of AR: it might be noticed that all the curves are now superimposed as, being that the shortest lengthscale  $H_o$  is constant, AR has no effect on the dynamics.

## C. Gel contraction velocity

We studied the contraction velocity of the lateral boundary of the disk, i.e., the radial velocity and the effects of AR on it. To do so, we evaluate the average radial stretch  $\Lambda_r$  as follows: 686

$$\Lambda_r(\tau) = 1 + \frac{1}{H_d} \int_0^{H_d} \frac{u(R_d, z, \tau)}{R_d} \, dz \,; \tag{42}$$

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it is easy to verify that the average stretch  $\Lambda_r$  also corresponds to the average  $\bar{\lambda}_r(\tau)$  of the radial deformation  $\lambda_r(r, z, \tau)$  on the cross section  $S_d$  of area  $R_d \cdot H_d$ .

We also defined an average current radius  $R(\tau)$  and a radial contraction velocity  $\dot{R}(\tau)$  with the formulas

$$R(\tau) = \Lambda_r(\tau)R_d$$
 and  $\dot{R}(\tau) = \Lambda_r(\tau)R_d$ . (43)

It follows from (43) and the definition of AR that the radial velocity can also be rewritten as  $\dot{R}(\tau) = \dot{\Lambda}_r(\tau) \frac{H_d}{2}$  AR. The radial velocity  $\dot{R}(\tau)$  is always negative, as the gel disk is contracting and negative is also the generalized force  $\beta$  that produces a contraction. So, in both Figs. 8 and 9 we represented  $-\dot{R}(\tau)$  and  $-\beta/\beta_0$ .

Figure 8 shows that, for a constant radius, the radial velocity  $\dot{R}(\tau)$  is characterized by two timescales, one for the time interval during which the velocity increases, and the second for the following interval where the velocity decreases. In the first time interval, the curves fit to a linear law, that is,  $\dot{R}(\tau) \propto \tau/\tau_r$ , with  $\tau_r$  the characteristic time of rising. 700



FIG. 8. The time evolution of  $\beta$  (dashed) and corresponding radial contraction velocity  $\vec{R}$  of the lateral boundary of the disk at constant radius  $R_o = 1.5$  mm for different values of AR; disk geometry is given in the first column of Table II. The color code is the same as in Figs. 6 and 7. The small wiggle in the blue line at  $\tau \simeq 17$  s is due to a mechanical buckling: the disk departs from the flat shape; see Fig. 12, panel (c). Velocity ranges over the left vertical axis and  $\beta/\beta_o$  over the right vertical axis.

During the decreasing time interval, curves fit to an ex-704 ponential law  $\dot{R}(\tau) \propto v_{\text{max}} \exp(-\tau/\tau_{\text{decay}})$ , with  $\tau_{\text{decay}}$  the 705 characteristic time of decay. The characteristic times of rising 706 and decay have been estimated for any aspect ratio and are 707 listed in Table III. 708

The inset in Fig. 8 shows that the maximum radial veloc-709 ity  $v_{\text{max}}$ , attained at peak time  $\tau_p$ , depends on the geometric 710 parameter AR [32]. 711

Actually, the analysis of Eqs. (42) and (43) shows that 712 when AR changes with  $H_d$  (or, equivalently, with  $H_o$  as the 713

 $H_o = \text{constant}$ 

120

100

80

60

40

20 25 30 35 40 45

AR

40

50

 $v_{max} (\mu m/s)$ 

20

10

FIG. 9. The time evolution of  $\beta$  (dashed) and corresponding radial contraction velocity  $\dot{R}$  of the lateral boundary of the disk at constant thickness  $H_a = 0.1$  mm for different values of AR; disk geometry is given in the second column of Table II. Color code is the same as in Figs. 6 and 7. Velocity ranges over the left vertical axis and  $\beta/\beta_o$  over the right vertical axis.

30

 $\tau(s)$ 

TABLE III. Max velocity  $v_{max}$ , peak time  $\tau_p$ , rising time  $\tau_r$ , and decay time  $\tau_{decay}$  for different values of aspect ratio AR.

AR	$v_{\rm max}~(\mu{ m m/s})$	$\tau_p(\mathbf{s})$	$\tau_r$ (s)	$\tau_{\rm decay}~({\rm s})$
20	44	$\simeq 16$	0.22	13
25	52	$\simeq 16$	0.22	13
30	74	$\simeq 17$	0.18	8
35	84	$\simeq 17$	0.14	3
40	104	$\simeq 17$	0.12	2
45	111	$\simeq 17$	0.11	1.5

initial free-swelling is homogeneous), with  $R_o$  constant, the 714 dependence of  $\vec{R}$  on AR is also affected by  $H_d$  and cannot 715 be linear. The same equations show that, for  $H_d$  constant, the 716 dependence of  $\hat{R}$  on AR is simply linear. This is what the inset 717 in Fig. 9 shows for the maximum velocity  $v_{\text{max}}$  relative to the 718 study at varying radius. 719

We can split the average stretch  $\Lambda_r$  into an elastic compo-720 nent  $\Lambda_e$  and an active component  $\Lambda_a$ , related to the analogous 721 decomposition of the deformation gradient  $\mathbf{F} = \mathbf{F}_e \mathbf{F}_a$  and of 722 the radial deformation  $\lambda_r$ . Thus, the stretching velocity  $\Lambda_r$  can 723 be written as the sum of two terms, and the radial velocity R724 is represented by 725

$$\dot{R} = (\dot{\Lambda}_a \Lambda_e + \Lambda_a \dot{\Lambda}_e) R_d, \qquad (44)$$

where  $\Lambda_a$  is the average of the active radial deformation  $\gamma_r$ , 726 and it depends on self-contraction, while  $\Lambda_e$  is the average of the elastic radial deformation  $\lambda_r/\gamma_r$ , and it depends on liquid transport.

Equation (44) highlights the existence of two timescales 730 for R: for  $\tau < \tau_{\beta}$  the stretching velocity is dominated by the 731 time evolution of  $\beta(\tau)$ , while for  $\tau > \tau_{\beta}$  it is dominated by 732 liquid transport, that is, 733

$$\dot{R} \simeq \Lambda_a \Lambda_e R_d \quad \tau < \tau_\beta,$$
 (45a)

$$\dot{R} \simeq \Lambda_a \dot{\Lambda}_e R_d \quad \tau > \tau_{\beta}.$$
 (45b)

Equation (45a) shows that for  $t < \tau_{\beta} = 20$  s, the radial veloc-734 ity  $\hat{R}$  changes with the same rate of  $\Lambda_a$ , which in turns depends 735 on  $\beta$ , as Figs. 8 and 9 show (compare the colored lines with 736 the dashed black line in both figures). 737

On the other side, Eq. (45b) shows that for  $t > \tau_{\beta} = 20$  s, 738 the radial velocity  $\hat{R}$  changes with the rate of  $\Lambda_e$ , which 739 depends on liquid transport and on the smallest lengthscale 740 of the disk, which in our case is  $H_{a}$ , as a comparison between 741 Figs. 8 and 9 shows. The same pair of figures also show clearly 742 that the maximal velocity is reached when  $\tau$  approaches  $\tau_{\beta}$ , 743 that is, when contraction is near to its maximum value-as 744 was suggested in [5] [see Fig. 4(f) in [5]]. 745

Finally, it is worth noting that the active control  $\beta$ , needed 746 to change the target mesh size, does not change further once it 747 has taken its maximal value. Beyond that, the system evolves 748 towards its steady state by releasing liquid until a new free 749 swollen configuration is reached; at this final state, the effects 750 of the network elasticity balance the active control. 751

We conclude this section by showing a comparison with 752 experimental results obtained for a very thin disk with 753 AR = 50. By properly tuning the diffusivity D and the dis-754 sipation  $\eta$ , our theoretical model is able to reproduce quite 755

-0.1

-0.2

-0.3

-0.4

-0.5

0.6

-0.7

-0.8

-0.9

60

727 728 729

-AR=45

AR = 40

AR=35

AR=30

AR=25

AR=20

110

100

90

80

70

60

50

40

30

20

10

0

 $-\dot{R}(\mu m/s)$ 



FIG. 10. Radial contraction velocities vs time. Radial  $\dot{R}$  (solid blue) contraction velocity of the disk compared with experimental data (dashed with markers). Disk geometry:  $R_o = 1.5$  mm, AR = 50; material parameters:  $D = 0.951 \times 10^{-4}$  m<sup>2</sup>/s,  $\eta = 1.51 \times 10^{5}$  Pa s.

well the time course of the radial contraction velocity  $\vec{R}$ . Figure 10 compares the predicted results (solid-blue) with the experimental ones (dashed-black, circle markers).

759

#### D. Densification and stress distribution

As observed in [5], the network starts contracting from the
boundary, and the actual mesh size starts decreasing from the
boundary to the center of the gel disk. This contraction mode
yields boundary effects, which are detected on the gel density,
defined as the ratio between the polymer mass and the overall
gel volume, and on the overall stress state in the disk.

In [5], a gel densification was observed, that is, an increase
 of the gel density starting at the periphery and propagating
 into the gel interior.

<sup>769</sup> Within the model, we use the ratio  $J_{d0}/J_d$  to measure the <sup>770</sup> densification from the initial state. Figure 11 shows the den-



FIG. 11. Densification at the middle cross section of the disk. Ratio  $J_{do}/J_d$  in the plane  $(R, \tau)$ ; color map: blue is more wet, red is more dry. Densification (red color) starts at the boundary and then propagates inward; disk radius contracts from  $R_o = 1.5$  mm to  $R_1 \simeq$ 0.55 mm.

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sification at the middle cross section of the disk by plotting 771 the ratio  $J_{d0}/J_d$  in the plane  $(R, \tau)$ , with R = r + u the cur-772 rent radial position. It is noted that, when  $\tau \equiv \tau_{\beta} = 20$  s and 773 contraction is fully developed, a narrow red strip of densifica-774 tion appears at the periphery; then, it propagates towards the 775 interior until the whole cross section is more dense. The repre-776 sentation in the current domain determines the peculiar "boot" 777 shape of the profile: as time goes on, the disk contracts and its 778 radius contracts from  $R_o = 1.5$  mm to  $R_1 \simeq 0.55$  mm. On the 779 other hand, stress analysis in the active disk can be relevant, as 780 overall stress distribution might drive mechanical instability, 781 which leads to a variety of different shapes at the end of 782 the contraction [5,20,33,34]. The analysis of instabilities is 783 beyond the scope of the present work, and it will mark our 784 future efforts. However, through the aforementioned studies, 785 we might have interesting clues about shape transitions by 786 investigating the effects of AR on the evolution of radial stress 787  $\sigma_r$  and the hoop one  $\sigma_{\theta}$  in the disk, which may drive further 788 experiments. 789

We only report results for the case of constant radius. We 790 compare the stress state in a thick (AR  $\simeq 20$ ) and a thin 791  $(AR \simeq 45)$  disk. Panels (a) and (b) of Fig. 12 show the ex-792 istence of two stress patterns: in a core region (beige), the 793 stress is constant along the radius and spherical, that is,  $\sigma_r =$ 794  $\sigma_{\theta}$ ; in the periphery (cyan), the stress varies with the radius 795 and  $\sigma_r \neq \sigma_{\theta}$ . As the bulk contraction  $\beta$  is homogeneous and 796 isotropic in the whole disk, these two regions are determined 797 by the dynamics of liquid transport. In particular, the width of 798 the peripheral region is of the order of the thickness because 799 the solvent in this region can escape from both the lateral 800 boundary and the top and bottom surfaces. In contrast, for 801 the solvent in the core, the shortest path to exit the gel disk 802 is through the top and bottom surfaces. Corresponding to our 803 values of AR, we have  $H_{\text{thin}} \simeq 0.04 R_d$  and  $H_{\text{thick}} = 0.1 R_d$ . 804

In particular, in Fig. 12, for AR = 20 we have essentially  $\sigma_r < 0$  along all the radius, and  $\sigma_{\theta}$  varying from negative to positive [see panel (a)]; for AR = 45 we have  $\sigma_r > 0$  along all the radius, and  $\sigma_{\theta}$  varying from positive to negative [see panel (b)]. The stress distribution for these two cases is typical of that found in frustrated domelike or saddlelike disks [see Fig. (12), panels (c) and (d)] [20,33,34].

That is a preliminary requirement for observing instability patterns that can deliver domes or saddles, depending on other key factors, which are not investigated in the present paper.

## E. Evolution of the aspect ratio during contraction

Finally, the geometry of the gel body suggests that we investigate the possibility of having dissipations  $\eta_r$  and  $\eta_{\theta}$  in the plane, different from the vertical dissipation  $\eta_z$ . Dissipations are related to the resistances of the mesh to reorganize, which can be expected to be different. Our conjecture needs to be validated, and the analysis may stimulate further experiments in this direction.

As noted at the end of Sec. II, the system is controlled by the pair  $(\mu_e, \beta)$ , and here we also analyze the combined effects of varying the chemical potential  $\mu_e$  and active force  $\beta$ (scenario b).

We always consider a homogeneous and isotropic generalized force  $\beta$ . Nevertheless, during gel contraction, the radial



FIG. 12. Effect of AR on stress distribution for disks with constant radius. Panels (a) and (b) show the radial  $\sigma_r$  (red) and hoop  $\sigma_\theta$  (blue) overall stresses vs the nondimensional radius  $r/R_d$  at  $\tau = 20$  s, for AR = 20 and 45. (a) AR = 20: the hoop stress is negative in the core (beige) and positive at the periphery (cyan), a typical pattern of frustrated domelike shape.

and vertical stretches might differ locally, and each one of them can vary in time and space. We use the average values  $R(\tau)$  and  $H(\tau)$  of radius and thickness to describe the change in the aspect ratio of the disk, with  $R(\tau)$  defined by Eq. (43) and  $H(\tau)$  defined as  $H(\tau) = \Lambda_z(\tau) H_d$  with

$$\Lambda_{z}(\tau) = 1 + \frac{1}{R_{d}} \int_{0}^{R_{d}} \frac{w(r, H_{d}, \tau)}{H_{d}} dr.$$
 (46)

At any time  $\tau$ , the ratio  $H(\tau)/H_o$  can be plotted against the 834 ratio  $R(\tau)/R_o$  to illustrate the evolution path of the radial and 835 vertical stretches, that is, the curve  $\tau \mapsto (R(\tau)/R_o, H(\tau)/H_o)$ , 836 plotted in the plane  $(R/R_o, H/H_o)$ . In Fig. 13, the curve has 837 been represented for a disk with AR = 22 and  $R_o = 1.5$  mm. 838 In that plot, the dashed line represents an isotropic evolution, 839 during which the aspect ratio remains constant during network 840 contraction. 841

For each of the two analyzed cases, corresponding to 842 scenario (a) (red) and (b) (blue), we show two curves, one 843 corresponding to equal dissipations (diamond markers),  $\eta_r =$ 844  $\eta_{\theta} = \eta_z$ , and the other with different horizontal and vertical 845 dissipations (asterisk markers),  $\eta_r = \eta_{\theta} = 2 \eta_z$ . We note that 846 the evolution is very sensitive to dissipation, while the dif-847 ferences between scenarios (a) and (b) are less noticeable. 848 For all simulations, the system evolves via a characteristic 849 path. It departs from the isotropic contraction path, but in 850 the case with equal dissipations the steady-state configuration 851 ends on the dashed line (i.e., on the isotropic path), while 852 the case with different dissipations ends far from it. In par-853 ticular, when  $\eta_r = \eta_z$ , the contraction is almost isotropic until 854  $H/H_o = R/R_o \sim 0.8$ ; then, the radial contraction is faster, and 855 eventually the vertical one becomes faster. When  $\eta_r = 2 \eta_z$ , 856 the vertical contraction is much faster than the radial one, and 857 the final state is not isotropic. 858

These first clues deserve to be investigated further both experimentally and numerically to stress the morphing chances of active gel.



FIG. 13. Thickness ratio  $H/H_o$  vs radius ratio  $R/R_o$  during contraction for cases (a) (red) and (b) (blue) with equal friction  $\eta_r = \eta_z$  (diamond) and differential friction  $\eta_r = 2 \eta_z$  (star);  $\eta_r = 10^5$  Pa s. The dashed line represents isotropic contractions; with different frictions, the radial and vertical contractions are not isotropic. Disk geometry:  $R_o = 1.5$  mm, AR = 22.

#### 862 VI. CONCLUSIONS AND FUTURE DIRECTIONS

We discussed the interplay between elasticity, liquid trans-863 port, and self-contractions in active gel disks from the 864 perspective of continuum mechanics. The transient problem 865 for gel disks of different aspect ratios has been solved, and dif-866 ferent aspects of the problem have been discussed: the regimes 867 of fast and slow liquid transport, the characteristic times of the contraction and liquid transport dynamics, and the changes in 869 the stress state in gel disks of different thickness. In doing so, 870 the analysis of the competitive role of gel contractility and 871 liquid flow in driving the mechanics of the active gel has been 872 exploited. 873

To keep the model easy, the numerical model has been de-874 veloped under the hypothesis of cylindrical symmetry, which 875 excludes the challenge to observe disk morphings, which are 876 not compatible with the cylindrical symmetry. Actually, we 877 are planning to give up the symmetry hypothesis above and 878 investigate the blossom of stresses in the disk, which may 879 drive instability patterns and, consequently, a variety of steady 880 shapes of the gel. This was beyond the scope of the present 881 work, and it will mark our future efforts. 882

Giving up the symmetry hypothesis also makes more interesting the identification of the determinants of possible changes in shape, whose control would make it possible to get actuators based on self-contractile gels, a promising field that can be set within the framework here presented.

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## APPENDIX

# 899 900

#### 1. Details of finite-element analysis

Equations (15), (16), and (22), together with the bound-901 ary (26) and initial (27) conditions, are rewritten in a weak 902 form and implemented in the software COMSOL MULTIPHY-903 ISICS by using the Weak-Form physics interface. The calculus 904 domain is the rectangular domain  $S_d$ , which is meshed with 905 triangular elements whose maximum mesh size is  $H_d/10$ , 906 yielding about 200 K DOFs. Lagrangian polynomials are 907 used as shape functions: polynomials of order 4 for the dis-908 placement and the solvent concentration, of order 3 for the 909 volumetric constraint, of order 2 for the boundary conditions 910 (also implemented in weak form), and of order 1 for the 911 remodeling variables. The whole set of coupled equations are 912 solved by using the Newton method with variable damping as 913 the nonlinear solver; the linear solver is the direct solver Par-914 diso, while the time-dependent solver uses the BDF method 915 with order 1-2. The time-dependent analysis starts at the 916 initial state  $\mathcal{B}_o$  and stops at a final equilibrium state  $\mathcal{B}_1$ , which 917 is preselected. 918

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